



# Backwashing in pressurized porous media filters: effects of porous media and underdrain design

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# Pressure sand filter in irrigation systems











Property	Units	Silica sand	Silica sand	Glass Microspheres
		(SS1)	(SS2)	(MS)
Grain size range	mm	0.75 - 0.85	0.63 - 0.75	0.63 - 0.75
Equivalent diameter $(d_{eq})$	mm	$0.922\pm0.019$	$0.715\pm0.015$	$0.652\pm0.014$
Particle density $(\rho_p)$	kg m-3	$2510\pm55$	$2410\pm12$	$2436.6 \pm 11$
Porosity $(\varepsilon)$	-	0.40	0.42	0.38
Sphericity coefficient ( $\psi$ )	-	0.89	0.89	1





a)











#### Nozzle 1 Nozzle 2 Nozzle 3 Nozzle 4 Nozzle 5 120% 8 100% 8 8 ଚ 80% 08 8 🗞 8 $\diamond$ 60% ø A Bed expansion (%) 40% 20% 0% A SS1 (0.75 - 0.85) 120% ♦ SS2 (0.63 - 0.75) • MS (0.63 - 0.75) 100% 80% Ч 60% 춛 40% 20% 0% 60 80 100 120 20 40 20 40 100 120 20 20 100 120 0 20 40 0 60 80 100 120 0 60 80 0 40 60 80 100 120 0 80

### Bed expansion results

Superficial velocity (m/h)





# Pressure drop ( $\Delta p$ ) results





Results





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methodology Results Discussion





# Conclusions

- An experimental study of the backwashing regime in a laboratory pressurized granular media filter was carried out for three different media types, two initial bed heights, and five different nozzles. The range of backflow superficial velocities analyzed included operating conditions similar to those encountered in commercial application.
- Video and data recordings of 820 backwashing tests were analyzed.
- The nozzle design plays a main role on the total pressure drop.
- The nozzle design influences the fluidized bed dynamics.
- The height of the expanded bed is mostly dependent on the media type.





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Effects of porous media type and nozzle design on the backwashing regime of pressurised porous media filters

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